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(54) Title: CONDUCTIVE POLYMER CURABLE CATHODE PASTE AND ELECTROLYTIC CELLS PRODUCED THEREFROM

(57) Abstract

This invention is directed to a cathode containing a cathodic material, a conducting polymer replacing carbon as the conductive material, a solid matrix forming monomer, a solvent, and a viscosifier, as well as electrolytic cells prepared from such solid cathodes.

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CONDUCTIVE POLYMER CURABLE CATHODE PASTE AND ELECTROLYTIC CELL. PRODUCED THEREFROM

BACKGROUND OF THE INVENTION

5 Field of the Invention

10 This invention is directed to a cathode paste containing a conductive polymer to replace carbon as the conductive material, and in particular, a cathode containing a cathodic material, a conductive polymer as the electroconductive material, a solid matrix forming monomer, a solvent and a viscosifier.

15 This invention is further directed to solid electrolytic cells (batteries) containing an anode, a solid electrolyte and a cathode containing a conductive polymer in place of carbon as the conductive material.

State of the Art

20 Electrolytic cells containing an anode, a cathode and a solid, solvent-containing electrolyte incorporating a salt are known in the art and are usually referred to as "solid batteries". These cells offer a number of advantages over electrolytic cells containing a liquid electrolyte (i.e., "liquid batteries") including improved safety features.

25 Notwithstanding their advantages, the manufacture of these solid batteries requires careful process controls to maximize the adherence of the various layers during formation of the electrolytic cells. Poorly adhered laminates can inhibit battery performance and can significantly reduce charge and discharge capacity.

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Specifically, solid batteries employ a solid electrolyte interposed between a cathode and an anode. The solid electrolyte contains either an inorganic or an organic matrix and a suitable salt, such as an inorganic ion salt, as a separate component. The inorganic matrix may be non-polymeric, e.g., β -alumina, silver oxide, lithium iodide, and the like, or polymeric, e.g., inorganic (polyphosphazene) polymers, whereas the organic matrix is typically polymeric. Suitable organic polymeric matrices are well known in the art and are typically organic polymers obtained by polymerization of a suitable organic monomer as described, for example, in U.S. Patent No. 4,908,283. Suitable organic monomers include, by way of example, ethylene oxide, propylene oxide, ethyleneimine, epichlorohydrin, ethylene succinate, and an acryloyl-derivatized alkylene oxide containing an acryloyl group of the formula $\text{CH}_2=\text{CR}'\text{C}(\text{O})\text{O}-$ where R' is hydrogen or a lower alkyl of from 1-6 carbon atoms.

Because of their expense and difficulty in forming into a variety of shapes, inorganic non-polymeric matrices are generally not preferred and the art typically employs a solid electrolyte containing a polymeric matrix. Nevertheless, electrolytic cells containing a solid electrolyte containing a polymeric matrix suffer from low ion conductivity and, accordingly, in order to maximize the conductivity of these materials, the matrix is generally constructed into a very thin film, i.e., on the order of about 25 to about 250 μm . As is apparent, the reduced thickness of the film reduces the total amount of internal resistance within the electrolyte thereby minimizing losses in conductivity due to internal resistance.

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The solid electrolytes also contain a solvent (plasticizer) which is typically added to the matrix primarily to enhance the conductivity of the electrolytic cell. In this regard, the solvent requirements of the solvent used in the solid electrolyte have been art recognized to be different from the solvent requirements in liquid electrolytes. For example, solid electrolytes require a lower solvent volatility as compared to the solvent volatilities permitted in liquid electrolytes.

Suitable solvents well known in the art for use in such solid electrolytes include, by way of example, propylene carbonate, ethylene carbonate, γ -butyrolactone, tetrahydrofuran, glyme (dimethoxyethane), diglyme, triglyme, tetraglyme, dimethylsulfoxide, dioxane, sulfolane and the like.

The solid, solvent containing electrolyte has typically been formed by one of two methods. In one method, the solid matrix is first formed and then a requisite amount of this material is dissolved in a volatile solvent. Requisite amounts of a salt, such as an inorganic ion salt, and the electrolyte solvent (typically a glyme compound and an organic carbonate) are then added to the solution. This solution is then placed on the surface of a suitable substrate, e.g., the surface of a cathode, and the volatile solvent is removed to provide for the solid electrolyte.

In the other method, a monomer or partial polymer of the polymeric matrix to be formed is combined with appropriate amounts of the salt and the solvent. This mixture is then placed on the surface of a suitable substrate, e.g., the surface of the cathode, and the monomer is polymerized or cured (or the partial polymer

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is then further polymerized or cured) by conventional techniques (heat, ultraviolet radiation, electron beams, and the like) so as to form the solid, solvent-containing electrolyte.

5 Typically, cathodes for solid electrolytic cells are prepared by coating a mixture of cathodic material, an electroconductive material such as carbon, a solid matrix forming monomer, a solvent, and a viscosifier on a current collector substrate followed by curing
10 with e-beam or UV radiation. In many cases it has been found that such mixtures are very difficult to apply at room temperature as a smooth even coating.

15 When the solid electrolyte is formed on a cathodic surface, an anodic material can then be laminated onto the solid electrolyte to form a solid battery, i.e., an electrolytic cell.

20 Regardless of which of the above techniques is used in preparing the electrolytic cell, improvements are sought in the processability of the cathode paste. Improvements in the conductivity of the components of the cathode paste are also sought to improve the conductivity of the solid cathode. Improvements in the cathode paste components are further sought in the application of lightweight materials which can be cast
25 into a smooth even coating or film.

30 In view of the above, the art is searching for methods to improve cathode manufacture, conductivity and coatability as well as to increase the adherence of the laminate layers of solid batteries employing such cathodes.

SUMMARY OF THE INVENTION

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5 The present invention is directed, in part, to the
discovery that the replacement of carbon as the
conductive material component of the cathode provides
for several benefits to the solid cathode manufacturing
process as well as to the solid battery itself. In
particular, the present invention provides for a
cathode wherein carbon is replaced by a conducting
polymer as the electronically conductive portion of the
cathode to increase the conductivity of the cathode
10 which provides for a cathode layer having improved
performance.

15 By replacing the carbon with a material having a
conductivity as good as, or better than carbon, the
conductivity of the entire cathode is improved. In
this manner, a solid cathode having improved electrical
properties is provided.

20 Further, an electrolytic cell having improved
mechanical properties is also provided. Replacing the
carbon with a lightweight material which can be readily
cast into a film improves the mechanical properties of
the electrolytic cell. Electrolytic cell manufacturing
procedures are also improved since laminate
construction is improved.

25 Moreover, the improved conductivity of the cathode
of the present invention improves battery performance.
Battery performance is improved by the addition of
conducting polymer materials which exhibit
conductivities over a wide range.

30 Accordingly, in one of its composition aspects,
the present invention is directed to a cathode for an
electrolytic cell which comprises:
a solid matrix forming monomer;

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a cathodic material;
an electroconductive material consisting of a
conducting polymer;
a solvent; and
5 a viscosifier.

In another of its composition aspects, the present invention is directed to an electrolytic cell which comprises:

10 an anode containing a compatible anodic material;
a cathode which comprises a solid polymeric matrix,
a cathodic material, an electroconductive material consisting of a conducting polymer, a solvent and a viscosifier; and
15 interposed therebetween a solid, solvent-containing electrolyte.

In one of its method aspects, the present invention is directed to a process for preparing a solid cathode for an electrolytic cell which comprises:

20 (a) providing a substrate;
(b) coating said substrate with a cathodic composition comprising: a solid matrix forming monomer, a cathodic material, an electroconductive material consisting of a conducting polymer, a solvent and a viscosifier; and
25 (c) curing said cathodic composition to provide a solid cathode.

In another of its method aspects, the present invention is directed to a process for preparing an
30 electrolytic cell which comprises:

(a) providing an anode containing a compatible anodic material;

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(b) providing a cathode comprising a solid polymeric matrix, a cathodic material, an electroconductive material consisting of a conducting polymer, a solvent and a viscosifier;

(c) interposing between surfaces of the cathode and the anode an electrolyte composition; and

(d) curing said electrolyte composition so as to provide a solid electrolyte bonded to the surfaces of both the anode and cathode.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

As noted above, this invention is directed to a cathode containing a conducting polymer replacing carbon as the electronically conductive portion of the cathode and, solid electrolytic cells made therefrom. By virtue of the conducting polymers employed, the increased conductivity of the components within the cathode is improved, which provides for a cathode layer having improved conductivity properties. The resultant improved cathode layer also provides for enhanced electrolyte performance. Electrolytic cell manufacturing procedures are also improved since the conducting is lightweight and readily cast into a film.

However, prior to describing this invention in further detail, the following terms are defined below.

Definitions

As used herein, the following terms have the following meanings.

The term "solid polymeric matrix" refers to an electrolyte compatible material formed by polymerizing

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an inorganic or organic monomer (or partial polymer thereof) and which, when used in combination with the other components of the electrolyte, renders the electrolyte solid. The solid matrix may or may not be ion-conducting.

Suitable solid polymeric matrices are well known in the art and include solid matrices formed from inorganic polymers, organic polymers or a mixture of organic polymers with inorganic non-polymeric materials. Preferably, the solid polymeric matrix is an organic matrix derived from a solid matrix forming monomer and from partial polymers of a solid matrix forming monomer.

Alternatively, the solid polymeric matrix can be used in combination with a non-polymeric inorganic matrix. See, for example, U.S. Patent No. 4,990,413, which is incorporated herein by reference in its entirety. Suitable non-polymeric inorganic materials for use in conjunction with the solid polymeric matrix include, by way of example, β -alumina, silver oxide, lithium iodide, and the like. Suitable inorganic monomers are also disclosed in U.S. Patent Nos. 4,247,499; 4,388,385; 4,414,607; 4,394,280; 4,432,891; 4,539,276; and 4,557,985 each of which is incorporated herein by reference.

The term "a solid matrix forming monomer" refers to inorganic or organic materials which in monomeric form can be polymerized, preferably in the presence of an inorganic ion salt, and a solvent mixture of an organic carbonate and a glyme compound, to form solid matrices which are suitable for use as solid electrolytes in electrolytic cells. Suitable solid matrix forming monomers are well known in the art and

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the particular monomer employed is not critical. Preferably, solid matrix forming monomers have at least one heteroatom capable of forming donor acceptor bonds with organic cations (e.g., alkali ions). When polymerized, such compounds form an ionically conductive matrix.

Examples of suitable organic solid matrix forming monomers include, by way of example, propylene oxide, ethyleneimine, ethylene oxide, epichlorohydrin, acryloyl-derivatized polyalkylene oxides (as disclosed in U.S. Patent No. 4,908,283), vinyl sulfonate polyalkylene oxides (as disclosed in U.S. Patent Application Serial No. 07/918,438, filed July 22, 1992, and entitled "SOLID ELECTROLYTES FORMED BY POLYMERIZATION OF VINYL SULFONATE POLYALKYLENE OXIDES" which application is incorporated herein by reference in its entirety), and the like as well as mixtures thereof.

Examples of suitable inorganic solid matrix forming monomers include, by way of example, phosphazenes and siloxanes. Phosphazene monomers and the resulting polyphosphazene solid matrix are disclosed by Abraham et al., Proc. Int. Power Sources Symp., 34th, pp. 81-83 (1990) and by Abraham et al., J. Electrochemical Society, Vol. 138, No. 4, pp. 921-927 (1991).

The term "a partial polymer of a solid matrix forming monomer" refers to solid matrix forming monomers which have been partially polymerized to form reactive oligomers. Partial polymerization may be conducted for the purpose of enhancing the viscosity of the monomer, decreasing the volatility of the monomer, and the like. Partial polymerization is generally

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permitted so long as the resulting partial polymer can be further polymerized, preferably in the presence of a solvent, such as, a mixture of an organic carbonate and a glyme compound, to form solid polymeric matrices which are suitable for use as solid electrolytes in electrolytic cells.

The term "cured" or "cured product" refers to the treatment of the solid matrix forming monomer or partial polymer thereof under polymerization conditions (including cross-linking) so as to form a solid polymeric matrix. Suitable polymerization conditions are well known in the art and include by way of example, heating the monomer, irradiating the monomer with UV light, electron beams, and the like. The resulting cured product preferably contains repeating units containing at least one heteroatom such as oxygen or nitrogen which is capable of forming donor acceptor bonds with inorganic cations (alkali ions). Examples of suitable cured products suitable for use in this invention are set forth in U.S. Patent Nos. 4,830,939 and 4,990,413 which are incorporated herein by reference in their entirety.

The solid matrix forming monomer or partial polymer can be cured or further cured prior to or after addition of the salt, solvent and viscosifier. For example, a composition comprising requisite amounts of the solid matrix forming monomer, salt, organic carbonate/glyme solvent and viscosifier can be applied to a substrate and then cured. Alternatively, the solid matrix forming monomer can be first cured and then dissolved in a suitable volatile solvent. Requisite amounts of the salt, organic carbonate/glyme solvent and viscosifier can then be added. The mixture is then placed on a substrate and cured; removal of the

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volatile solvent would result in the formation of a solid electrolyte. In either case, the resulting solid electrolyte would be a homogeneous, single phase product which is maintained upon curing, and does not readily separate upon cooling to temperatures below room temperature. Accordingly, the solid electrolyte of this invention does not include a separator as is typical of liquid electrolytes.

The term "salt" refers to any salt, for example, an inorganic salt, which is suitable for use in a solid electrolyte. Representative examples of suitable inorganic ion salts are alkali metal salts of less mobile anions of weak bases having a large anionic radius. Examples of such anions are I^- , Br^- , SCN^- , ClO_4^- , BF_4^- , PF_6^- , AsF_6^- , CF_3COO^- , $CF_3SO_3^-$, and the like. Specific examples of suitable inorganic ion salts include $LiClO_4$, LiI , $LiSCN$, $LiBF_4$, $LiAsF_6$, $LiCF_3SO_3$, $LiPF_6$, $(CF_3SO_2)_2NLi$, $(CF_3SO_2)_3CLi$, NaI , $NaSCN$, KI and the like. The inorganic ion salt preferably contains at least one atom selected from the group consisting of Li, Na and K.

The term "organic carbonate" refers to hydrocarbyl carbonate compounds of no more than about 12 carbon atoms and which do not contain any hydroxyl groups. Preferably, the organic carbonate is a linear aliphatic carbonate and most preferably a cyclic aliphatic carbonate.

Suitable cyclic aliphatic carbonates for use in this invention include 1,3-dioxolan-2-one (ethylene carbonate); 4-methyl-1,3-dioxolan-2-one (propylene carbonate); 4,5-dimethyl-1,3-dioxolan-2-one; 4-ethyl-1,3-dioxolan-2-one; 4,4-dimethyl-1,3-dioxolan-2-one; 4-methyl-5-ethyl-1,3-dioxolan-2-one; 4,5-diethyl-1,3-dioxolan-2-one; 4,4-diethyl-1,3-

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dioxolan-2-one; 1,3-dioxan-2-one; 4,4-dimethyl-1,3-dioxan-2-one; 5,5-dimethyl-1,3-dioxan-2-one; 5-methyl-1,3-dioxan-2-one; 4-methyl-1,3-dioxan-2-one; 5,5-diethyl-1,3-dioxan-2-one; 4,6-dimethyl-1,3-dioxan-2-one; 4,4,6-trimethyl-1,3-dioxan-2-one; and spiro (1,3-oxa-2-cyclohexanone-5',5',1',3'-oxa-2'-cyclohexanone).

Several of these cyclic aliphatic carbonates are commercially available such as propylene carbonate and ethylene carbonate. Alternatively, the cyclic aliphatic carbonates can be readily prepared by well known reactions. For example, reaction of phosgene with a suitable alkane- α,β -diol (dihydroxy alkanes having hydroxyl substituents on adjacent carbon atoms) or an alkane- α,γ -diol (dihydroxy alkanes having hydroxyl substituents on carbon atoms in a 1,3 relationship) yields an a cyclic aliphatic carbonate for use within the scope of this invention. See, for instance, U.S. Patent No. 4,115,206, which is incorporated herein by reference in its entirety.

Likewise, the cyclic aliphatic carbonates useful for this invention may be prepared by transesterification of a suitable alkane- α,β -diol or an alkane- α,γ -diol with, e.g., diethyl carbonate under transesterification conditions. See, for instance, U.S. Patent Nos. 4,384,115 and 4,423,205 which are incorporated herein by reference in their entirety.

Additional suitable cyclic aliphatic carbonates are disclosed in U.S. Patent No. 4,747,850 which is also incorporated herein by reference in its entirety.

The term "viscosifier" refers to a suitable viscosifier for solid electrolytes. Viscosifiers

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include conventional viscosifiers such as those known to one of ordinary skill in the art. Suitable viscosifiers include film forming agents well known in the art which include, by way of example, polyethylene oxide, polypropylene oxide, copolymers thereof, and the like, having a number average molecular weight of at least about 100,000, polyvinylpyrrolidone, carboxymethylcellulose, and the like.

The term "electrolytic cell" refers to a composite containing an anode, a cathode and an ion-conducting electrolyte interposed therebetween.

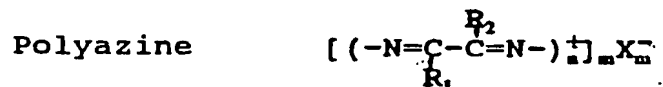
The anode is typically comprised of a compatible anodic material which is any material which functions as an anode in a solid electrolytic cell. Such compatible anodic materials are well known in the art and include, by way of example, lithium, lithium alloys such as alloys of lithium with aluminum, mercury, tin, zinc, and the like, and intercalation based anodes such as carbon, tungsten oxides and the like.

The cathode is comprised of a compatible cathodic material, i.e., insertion compounds, which is any material which functions as a positive pole in a solid electrolytic cell. Such compatible cathodic materials are well known in the art and include, by way of example, manganese oxides, molybdenum oxides, vanadium oxides, sulfides of titanium, molybdenum and niobium, lithiated cobalt oxides, lithiated manganese oxides, lithiated nickel oxides, chromium oxides, copper oxides, and the like. The particular compatible cathodic material employed is not critical.

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The compatible cathodic material is further mixed with an electronically conductive polymer, e.g., characterized by a conjugated network of double bonds, and a binder, such as a polymeric binder, to form under pressure a positive cathodic plate. The conductive polymer replaces all of the typically present electroconductive material including, by way of example, graphite, powdered carbon, powdered nickel, metal particles and the like. Suitable conductive polymers include polypyrrole, polyacetylene, polyazine, polyaniline, polyparaphenylene, polythiophene and the like. Examples of conductive polymers in oxidized form include the following shown:

Polyacetylene $[(-CH=CH-)_{n+}]_m X_m^-$ i.e., where n is an integer from about 10 to about 5000 and m is an integer between about 1 and about 1000.



where R_1 and R_2 are C_1 - C_6 alkyl or alkoxy groups such as CH_3 , CH_2CH_3 , and the like.

Polythiophene $[(2,5\text{-thiophenediyl})_{n+}]_m X_m^-$

where $X^- = ClO_4^-$, PF_6^- , BF_4^- , ASF_6^- , I^- , I_3^- , I_5^- , and the like.

Polypyrrole $[(2,5\text{-pyrrolediyl})_{n+}]_m X_m^-$

Polyparaphenylene $[(1,4\text{-phenylene})_{n+}]_m X_m^-$

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Organic electronically conducting polymers are a class of materials known to exhibit conductivities over a large range, e.g., 10-15 orders of magnitude, depending on the specific material chosen and the extent of doping. This range extends from the insulator state of the unmodified organic polymeric material through the semiconducting regime and extending into the highly conducting metallic state. A desirable feature of conducting polymers is that they are light weight materials that can be readily cast into films.

Typically, depending upon the method of synthesis, conducting polymers are produced in a nonconductive form and must be doped with either oxidizing agents or reducing agents to activate the conducting properties. Organic polymeric materials are reacted with electron donor or acceptor molecules to modify their room temperature electrical conductivity. The electron donor or acceptor molecules, generally known in the art as n-type and p-type dopants respectively, can transform the organic polymeric materials so that these modified organic polymeric materials exhibit semiconducting and metallic room temperature electrical conductivity. Polyacetylene is an example of an organic polymeric material whose room temperature electrical conductivity can be modified over several orders of magnitude above its insulator state, by the incorporation of dopant molecules, see U.S. Patent No. 4,222,903, which is incorporated herein by reference in its entirety. Other examples of organic polymeric materials whose room temperature electrical conductivity can be enhanced by several orders of magnitude over their insulator state by means of incorporation of dopant molecules are poly-p-phenylene, polypyrrole, poly-1,6 heptadiyne, and polyphenylene

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vinylene. Still other conducting polymers and methods are disclosed in U.S. Patents 4,519,939; 4,519,940; 4,522 and 4,579,679 the disclosure of each of which is incorporated herein in its entirety.

5 Electronically conducting polymers have a conductivity which has been modified with electron acceptor or donor dopants to be greater than the conductivity of the virgin state of the polymer. The electroactive organic polymeric material is fabricated
10 from a virgin polymer, by modifying the polymer with electron donor dopants or electron acceptor dopants. An n-type electroactive organic polymer is obtained by reacting the virgin polymer with reducing or electron donor dopants. Electron donor dopants induce n-type
15 conductivity in the polymer by donating electrons to the polymer and reducing the polymer to a polyanion and the dopant is oxidized to a charge neutralizing cation. Similarly, a p-type electroactive organic polymer is obtained by reacting the virgin polymer with oxidizing
20 electron acceptor dopants. Electron acceptor dopants induce p-type conductivity in the polymer by oxidizing the polymer to a polycation and the dopant is reduced to a charge neutralizing anion.

25 Alternatively, the polymers can be oxidized or reduced to their conductive form using electrochemical techniques. In this method, also known as electrochemical doping, the polymer is immersed in a suitable electrolyte solution and used as one electrode of an electrochemical cell. Upon passing an electric
30 current through the cell, the polymer is reduced or oxidized (depending upon the direction of current flow) and charge compensating cationic or anionic dopants from the supporting electrolyte are incorporated into the polymer. For both types of doping, the resulting

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5 electroactive polymer consists of a charged polymer backbone incorporating charge compensating ionic dopants. The charges of the polymer and the charge compensating dopants balance so that the electroactive polymer is electrically neutral. The oxidation or reduction proceeds by an electron transfer.

10 The desired value of the room temperature electrical conductivity of the dopant modified electroactive organic polymer can be adjusted by controlling the level of incorporation of the dopants into the virgin polymer. Alternatively, the desired value of the room temperature electrical conductivity of the dopant modified electroactive organic polymer is preselected by controlling the length of the reaction time between the virgin polymer and dopants.

20 In a preferred embodiment, the cathode is prepared from a cathode paste which comprises from about 35 to 65 weight percent of a compatible cathodic material; from about 1 to 20 weight percent of a conducting polymer; from about 0 to 20 weight percent of polyethylene oxide having a number average molecular weight of at least 100,000; from about 10 to 50 weight percent of solvent comprising a 10:1 to 1:4 (w/w) mixture of an organic carbonate and a glyme; and from about 5 weight percent to about 30 weight percent of a solid matrix forming monomer or partial polymer thereof. (All weight percents are based on the total weight of the cathode.)

30 The cathode paste can be prepared and injected between a pair of rollers with a piece of metal foil on the bottom that later acts as one of the battery components and a piece of plastic covered material on the top. The cathode paste is ejected out of a tube

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between these two rollers and the distance between the rollers can be adjusted or a knife blade or the like can be employed to provide the desired thickness of the coating on the metal substrate.

5 The cathode paste is typically spread onto a suitable support such as a current collector and then cured by conventional methods to provide for a solid positive cathodic plate. The cathode (excluding the support) has a thickness of about 20 to about 120
10 microns, preferably 75 microns.

 Current collectors are well known in the art, some of which are commercially available. A particularly preferred current collector for the cathode is a roughened nickel (electrolytically deposited nickel) on
15 nickel current collector (available as CF18/NiT from Fukuda Metal Foil & Powder Company, Ltd., Kyoto, Japan). The current collectors are preferably attached to the surface of the cathode not facing the electrolyte but can also be attached to the anode.
20 When the current collector is attached to the cathode, the cathode is interposed between the electrolyte and the current collector.

 In still another preferred embodiment, the electrolyte solvent and the cathode solvent are
25 identical.

Methodology

 Methods for preparing solid, solvent-containing electrolytes are well known in the art. In one embodiment, this invention utilizes a particular
30 solvent (plasticizer) mixture in the preparation of solid electrolytes.

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As noted above, organic carbonates are either commercially available or can be prepared by art recognized methods. For example, the preparation of carbonate compounds can be readily prepared by reaction of an ethylene oxide derivative with ROH under polymerization conditions. See, for example, U.S. Patent No. 4,695,291 which is incorporated herein by reference in its entirety.

The solid, solvent-containing electrolyte can be preferably prepared by combining, for example, a solid matrix-forming monomer with a salt, the solvent mixture of an organic carbonate and a glyme and a viscosifying agent. The resulting composition can then be uniformly coated onto a suitable substrate, e.g., aluminum foil, a glass plate, a lithium anode, a cathode, interposed between an anode and a cathode, and the like, by means of a roller, a doctor blade, a bar coater, a silk screen or spinner to obtain a film of this composition or its solution prior to curing. In some cases, it may be necessary to heat the composition so as to provide for a coatable material.

Preferably, the amount of material coated onto the substrate is an amount sufficient so that after curing, the resulting solid, solvent-containing electrolyte has a thickness of no more than about 250 microns (μm). More preferably, the solid, solvent-containing electrolyte may have a thickness of from about 25 to about 100 microns. The final thickness will depend on the particular application.

The electrolyte composition typically comprises from about 5 to about 25 weight percent salt, based on the total weight of the electrolyte; preferably from

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about 10 to 20 weight percent; and even more preferably from about 10 to about 15 weight percent.

5 The electrolyte composition typically comprises from about 40 to about 80 weight percent solvent, based on the total weight of the electrolyte; preferably from about 60 to about 80 weight percent; and even more preferably about 70 weight percent.

10 The solid electrolyte composition typically comprises from about 5 to about 30 weight percent of solid polymeric matrix, based on the total weight of the electrolyte; preferably from about 15 to about 25 weight percent.

15 The solid electrolyte composition typically comprises from about 1 to about 15 weight percent of a viscosifier, based on the total weight of the electrolyte composition. Preferably, the viscosifier is employed in an amount of from about 1 to about 10 weight percent, and more preferably from about 2 to about 5 weight percent based on the total weight of the
20 electrolyte composition.

25 The composition can be cured by conventional methods to form a solid film. For example, when the solid matrix forming monomer contains a reactive double bond, suitable curing methods include heating, irradiation with UV radiation, irradiation with
30 electron beams (EB), and the like. When the composition is cured by heating or UV radiation, the composition preferably contains an initiator. For example, when curing is by heating, the initiator is typically a peroxide such as benzoyl peroxide, methyl ethyl ketone peroxide, t-butyl peroxypropionate, diisopropyl peroxydicarbonate, and the like. When curing

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is by UV radiation, the initiator is typically benzophenone, Darocur 1173 (Geigy, Ardlesy, New York), and the like.

5 The initiator is generally employed in an amount sufficient to catalyze the polymerization reaction. Preferably, the initiator is employed at up to about 1 weight percent, based on the weight of the solid matrix forming monomer. When curing is by EB treatment, an initiator is not required.

10 In an alternative embodiment, the solid polymeric matrix, e.g., formed by polymerization of a solid matrix forming monomer, can be dissolved in a suitable volatile solvent and the requisite amounts of, for
15 example, the salt, solvent mixture of an organic carbonate and a glyme, and viscosifier are then added. The mixture can then be applied onto a suitable substrate, e.g., the surface of the cathode opposite to the current collector, an anode, interposed between an
20 anode and a cathode, and the like, in the manner set forth above. The volatile solvent can be removed by conventional techniques and the composition cured, which should provide for a solid electrolyte. Suitable
25 volatile solvents preferably have a boiling point of less than 85°C and more preferably between about 45°C and about 85°C. Particularly preferred volatile solvents are aprotic solvents. Examples of suitable volatile solvents include acetonitrile, tetrahydrofuran, and the like. However, acetonitrile is not preferred if it is to contact a metallic anode.

30 The resulting solid electrolyte should be a homogeneous, single-phase material which is maintained upon curing, and does not readily separate upon cooling to temperatures below room temperature. See, for example,

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U.S. Patent No. 4,925,751 which is incorporated herein by reference in its entirety.

5 Additionally, it is desirable to avoid the use of
any protic materials which will be incorporated into
the battery. For example, most of the protic
10 inhibitors in mono-, di-, tri- and higher functional
acrylate monomers as well as in the urethane acrylate
prepolymers, are preferably removed prior to formation
of the cathode and/or electrolyte. In this regard,
15 removal of these inhibitors down to a level of less
than 50 parts per million (ppm) can be accomplished by
contacting these monomers and prepolymers with an
inhibitor remover. Suitable inhibitor removers are
commercially available.

15 In a preferred embodiment, the process of forming
an electrolytic cell comprises the steps of coating the
surface of a current collector with a cathode paste
containing a cathodic material, a conducting polymer, a
20 solid matrix forming monomer, a solvent and a
viscosifier and curing the composition. The cathode
can then be coated with an electrolyte composition.
The electrolyte composition can then be cured to
provide for a solid electrolyte on the cathodic
25 surface. The anode, e.g., a lithium foil, can then be
laminated to this composite product in such a way that
the solid electrolyte is interposed between the lithium
foil and the cathode. In this manner, the cathode
conducting polymer can increase the conductivity of the
30 cathode components and improve the coatability of the
cathode paste, to provide a solid cathode and
electrolytic cell having improved properties.

 In a further preferred embodiment, this process
can be reversed, so that the surface of an anode, is

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coated with an electrolyte composition. The composition
can then be cured to provide for a solid electrolyte on
the anodic surface. The cathode paste can then be
coated and cured on this composite product in such a
way that the solid electrolyte is interposed between
the composite anodic material and the cathodic
material. In this manner, the cathode conducting
polymer can increase the conductivity of the cathode
components and improve the coatability of the cathode
paste, to provide a solid cathode and electrolytic cell
having improved properties.

In a further embodiment, the process of forming an
electrolytic cell comprises the steps of interposing an
electrolyte composition between the surfaces of an
anode and a cathode containing a cathodic material, a
conducting polymer, a solid polymeric matrix, a
solvent, and a viscosifier. The composition can then
be cured to provide for a solid electrolyte interposed
between the cathodic and anodic surface. In this
manner, the cathode conducting polymer can increase the
conductivity of the cathode components and improve the
coatability of the cathode paste, to provide a solid
cathode and electrolytic cell having improved
properties.

Methods for preparing solid electrolytes and
electrolytic cells are also set forth in U.S. Patent
Nos. 4,830,939 and 4,925,751 which are incorporated
herein by reference in their entirety.

Utility

The present invention, in view of the discussion
above, achieves the following:

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The conducting polymer-containing cathode paste described herein is particularly useful in preparing a solid cathode wherein the cathode paste has improved film forming properties and in preparing a solid electrolytic cell produced therefrom having improved performance.

The conducting polymer-containing cathode paste described herein is also particularly useful in preparing a solid cathode wherein the conducting polymer contributes to the conductivity of the cathode, improving the conductivity of the electrolytic cell produced therefrom.

In addition, the conducting polymer-containing cathode paste described herein has improved processing properties which include the ability to be applied in a smooth even lightweight coating.

The following prophetic examples are offered to illustrate the present invention and should not be construed in any way as limiting its scope.

EXAMPLE 1

A. The Cathode

The cathode may be prepared from a cathodic paste which, in turn, may be prepared from a cathode powder as follows:

i. Cathode Powder

The cathode powder can be prepared by placing V_6O_{13} (prepared by heating ammonium metavanadate ($NH_4^+VO_3^-$) at $450^\circ C$ for 16 hours under N_2 flow) into a grinding

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machine (Attritor Model S-1 purchased from Union Process, Akron, Ohio) and ground for 45 minutes. Afterwards, the resulting mixture can be dried at about 260°C for 16 hours under vacuum.

5

ii. Cathode Paste

A cathode paste may be prepared by combining sufficient cathode powder which should provide for a final product having 45 weight percent V_6O_{13} .

10

Specifically, about 225 grams of ground V_6O_{13} and about 50.1 grams of an alkylpolythiophene can be combined in a glove box (under dry (<10 ppm H_2O) argon at ambient temperature and pressure) with about 169.9 grams of a 4:1 w/w mixture of propylene carbonate/triglyme (triglyme is commercially available from Aldrich Chemical Company) and the resulting composite mixed under dry argon and at ambient temperature and pressure on a double planetary mixer (Ross #2 mixer available from Charles Ross & Sons, Company, Hauppauge, New York) at about 25 rpms until a paste is formed.

15

20

25

30

About 5 grams of polyethylene oxide (number average molecular weight about 600,000 available as Polyox WSR-205 from Union Carbide Chemicals and Plastics, Danbury, CT), about 42.5 grams of polyethylene glycol diacrylate (molecular weight about 500 available as SR-344 from Sartomer Company, Inc., Exton, PA) and containing less than about 50 ppm of inhibitor, and about 7.5 grams of ethoxylated trimethylpropane triacrylate (TMPEOTA) (molecular weight about 425 available as SR-454 from Sartomer Company, Inc., Exton, PA) and containing less than about 50 ppm of inhibitor can be added to the mixer.

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The resulting slurry in the mixer can be heated at about 65°C while mixing for 2 hours at 60 rpms to provide for the cathodic paste which would have the following approximate weight percent of components:

5	V ₆ O ₁₃	45.0	weight percent
	3-alkylpolythiophene	10.0	weight percent
	propylene carbonate	28.0	weight percent
	Triglyme	6.0	weight percent
	Polyethylene glycol		
10	diacrylate	8.5	weight percent
	Ethoxylated trimethylpropane		
	triacylate ¹	1.5	weight percent
	Polyethylene oxide	1.0	weight percent

15 In an alternative embodiment, the requisite amounts of all of the cathodic materials other than the cathode powder can be combined to form a first mixture and this first mixture is combined with the cathode powder to form a second mixture. This second mixture can be then thoroughly mixed to provide for the cathode
20 paste.

The cathode paste which can be prepared as above can be placed onto a sheet (about 1 mil (N-25 μm) thick by 10 cm wide) of a roughened nickel on nickel current collector (available as CF18/NiT from Fukuda Metal Foil
25 & Powder Company, Ltd., Kyoto, Japan). A Mylar cover sheet can then be placed over the paste and the paste spread to a thickness of about 75 microns (μm) with a

¹ Inhibitor may be removed from both the polyethylene glycol diacrylate and ethoxylated
30 trimethylpropane triacylate by contacting each of these compounds with an Inhibitor Remover available as Product No. 31,133-2 from Aldrich Chemical, Milwaukee, Wisconsin, which results in less than 50 ppm of inhibitor in the product.

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conventional plate and roller system and cured by continuously passing the sheet through an electron beam apparatus (Electrocurtain, Energy Science Inc., Woburn, MA) at a voltage of about 175 kV and a current of about 12 mA and at a conveyor belt speed setting of 50 which provides a conveyor speed of about 3 in/sec. After curing, the Mylar sheet can be removed which should provide for a solid cathode laminated to a nickel on nickel current collector.

B. Electrolyte

The electrolyte may be prepared by first combining 52 grams of propylene carbonate, 13 grams of triglyme and 17 grams of urethane acrylate (available as Photomer 6140 from Harckos, Manchester, U.K.). The propylene carbonate/triglyme/urethane acrylate mixture can be dried over molecular sieves (Grade 514, 4A, 8-12 mesh, available from W. R. Grace, Baltimore, MD) to remove water.

This solution can then be combined with 3 grams of polyethylene oxide (weight average molecular weight about 600,000 available as Polyox WSR-205 from Union Carbide Chemicals and Plastics, Danbury, CT). The mixture can then be thoroughly mixed with the same laboratory mixer at heating until a temperature of about 65°C is reached and then cooled to ambient temperature over at least a 2 hour period while stirring is maintained.

Once the polyethylene oxide is dispersed and dissolved, 5 grams of LiPF_6 (available from Hashimoto Chemical Corporation, Osaka Japan), 5 grams of $\text{Li}(\text{OCH}_2\text{CH}_2)_3\text{OCH}_3$ can be added while stirring with a laboratory mixer (Yamato Model LR41B, available from

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Fisher Scientific, Santa Clara, CA). The $\text{Li}(\text{OCH}_2\text{CH}_2)_3\text{OCH}_3$ salt can be prepared from a 1:1 molar ratio n-butyl lithium and the monomethylether of triethylene glycol in tetrahydrofuran at -78°C . Other aprotic solvents could also be used.

The resulting 100 gram mixture would contain the following weight percent of components:

Propylene carbonate	52	weight percent
Triglyme	13	weight percent
Urethane acrylate (Photomer 6140)	17	weight percent
LiPF_6	10	weight percent
Polyethylene oxide	3	weight percent

Afterwards, the electrolyte mixture can then be coated by a conventional knife blade to a thickness of about $50\text{ }\mu\text{m}$ onto the surface of the cathode sheet prepared as above (on the side opposite that of the current collector) but without the Mylar covering. The electrolyte can then be cured by continuously passing the sheet through an electron beam apparatus (Electrocurtain, Energy Science Inc., Woburn, MA) at a voltage of about 175 kV and a current of about 1.0 mA and at a conveyor speed setting of 50 which provides for a conveyor speed of about 1 cm/sec. After curing, a composite is recovered which should contain a solid electrolyte laminated to a solid cathode which, in turn, is laminated to a nickel on nickel current collector.

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C. Anode

5 The anode may comprise a sheet of lithium foil (about 51-76 μm thick) which is commercially available from FMC Corporation Lithium Division, Bessemer City, NC.

D. The Solid Battery

10 A solid battery may be prepared by first preparing a cathodic paste as described above which can be spread onto a substrate, e.g., a current collector, and then cured to provide the cathode. An electrolyte composition as described above can then be placed onto the cathode surface and cured to provide for the solid electrolyte. Then, the anode can be laminated onto the solid electrolyte to provide for the solid battery.

EXAMPLE 2

15 A solid electrolytic cell can be prepared by first preparing a cathodic paste which is spread onto a current collector and cured to provide for the cathode. An electrolyte solution can be placed onto the cathode surface and cured to provide for the solid electrolyte composition. Then, the anode can be laminated onto the solid electrolyte composition to provide for a solid electrolytic cell. The specifics of this construction are as follows:

25 A. The Current Collector

The current collector is a sheet of aluminum foil having a layer of adhesion promoter attached to the surface of the foil which should contact the cathode so as to form a composite having a sheet of aluminum foil,

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a cathode and a layer of adhesion promoter interposed therebetween.

Specifically, the adhesion promoter layer can be prepared as a dispersed colloidal solution by one of two methods. The first preparation of this colloidal solution for this example can be as follows:

84.4 weight percent of carbon powder
(Shawinigan Black™ -- available from Chevron Chemical Company, San Ramon, CA)

337.6 weight percent of a 25 weight percent solution of polyacrylic acid (a reported average molecular weight of about 90,000, commercially available from Aldrich Chemical Company -- contains about 84.4 grams polyacrylic acid and 253.2 grams water)

578.0 weight percent of isopropanol

The carbon powder and isopropanol can be combined with mixing in a conventional high shear colloid mill mixer (Ebenbach-type colloid mill) until the carbon is uniformly dispersed and the carbon particle size is smaller than 10 microns. At this point, the 25 weight percent solution of polyacrylic acid can be added to the solution and mixed for approximately 15 minutes. The resulting mixture can be pumped to the coating head and roll coated with a Meyer rod onto a sheet of aluminum foil (about 9 inches wide and about 0.0005 inches thick). After application, the solution/foil can be contacted with a Mylar wipe (about 0.002 inches thick by about 2 inches and by about 9 inches wide -- the entire width of aluminum foil). The wipe can be flexibly engaged with the foil, i.e., the wipe contacts the foil, to redistribute the solution so as to provide for a substantially uniform coating. Evaporation of the solvents, i.e., water and isopropanol, via a conventional gas-fired oven can provide for an

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electrically conducting adhesion-promoter layer of about 6 microns in thickness or about 3×10^{-4} grams per cm^2 . The aluminum foil can be cut to about 8 inches wide by removing approximately $\frac{1}{2}$ inch from either side by the use of a conventional slitter so as to remove any uneven edges.

In order to further remove the protic solvent from this layer, the foil can be redried. In particular, the foil can be wound up and a copper support can be placed through the roll's cavity. The roll can be hung overnight from the support in a vacuum oven maintained at about 130°C . Afterwards, the roll can be removed. In order to avoid absorption of moisture from the atmosphere, the roll can be preferably stored in a desiccator or other similar anhydrous environment to minimize atmospheric moisture content until the cathode paste is ready for application onto this roll.

The second preparation of this colloidal solution can comprise mixing 25 lbs of carbon powder (Shawinigan Black™ -- available from Chevron Chemical Company, San Ramon, CA) with 100 lbs of a 25 weight percent solution of polyacrylic acid (average molecular weight of about 240,000, commercially available from BF Goodrich, Cleveland, Ohio, as Good-Rite K702 -- contains about 25 lbs polyacrylic acid and 75 lbs water) and with 18.5 lbs of isopropanol. Stirring can be done in a 30 gallon polyethylene drum with a gear-motor mixer, e.g., Lightin Labmaster Mixer, model XJ-43, available from Cole-Parmer Instruments Co., Niles, Illinois, at 720 rpm with two 5 inch diameter A310-type propellers mounted on a single shaft. This procedure can wet down the carbon and eliminate any further dust problem. The

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resulting weight of the mixture should be about 143.5 lbs and contain some "lumps".

5 The mixture can be further mixed with an ink mill which consists of three steel rollers almost in contact with each other, turning at 275, 300, and 325 rpms, respectively. This high shear operation allows particles that are sufficiently small to pass directly through the rollers. Those that do not pass through the rollers can continue to mix in the ink mill until
10 they are small enough to pass through these rollers. When the mixing is complete, the carbon powder is completely dispersed. A Hegman fineness of grind gauge (available from Paul N. Gardner Co., Pompano Beach, FL) should indicate that the particles are 4-6 μm with the
15 occasional 12.5 μm particles. The mixture can be stored for well over 1 month without the carbon settling out or reagglomerating.

20 When this composition is to be used to coat the current collector, an additional 55.5 lbs of isopropanol can be mixed into the composition working with 5 gallon batches in a plastic pail using an air powered shaft mixer (Dayton model 42231 available from Granger Supply Co., San Jose, CA) with a 4 inch diameter Jiffy-Mixer brand impeller (such as an
25 impeller available as Catalog No. G-04541-20 from Cole Parmer Instrument Co., Niles, Illinois). The composition can be gear pumped through a 25 μm cloth filter, e.g., So-Clean Filter Systems, American Felt and Filter Company, Newburgh, NY, and Meyer-rod coated
30 as described above.

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B. The Cathode

The cathode can be prepared from a cathodic paste which, in turn, can be prepared from a cathode powder as follows:

5

i. Cathode Powder

10

The cathode powder can be prepared by placing V_6O_{13} (prepared by heating ammonium metavanadate ($NH_4^+VO_3^-$) at $450^\circ C$ for 16 hours under N_2 flow) into a grinding machine (Attritor Model S-1 purchased from Union Process, Akron, Ohio) and ground for 30 minutes. Afterwards, the resulting mixture can be dried at about $260^\circ C$ for 21 hours.

ii. Cathode Paste

15

A cathode paste can be prepared by combining sufficient cathode powder which should provide for a final product having 45 weight percent V_6O_{13} .

20

Specifically, 171.6 grams of a 4:1 weight ratio of propylene carbonate:triglyme can be combined with 42.9 grams of polyethylene glycol diacrylate (molecular weight about 400 available as SR-344 from Sartomer Company, Inc., Exton, PA), and about 7.6 grams of ethoxylated trimethylolpropane triacrylate (TMPEOTA) (molecular weight about 450 available as SR-454 from Sartomer Company, Inc., Exton, PA) in a double planetary mixer (Ross #2 mixer available from Charles Ross & Sons, Company, Hauppauge, New York).

25

A propeller mixture can be inserted into the double planetary mixer and the resulting mixture can be stirred at 150 rpms until homogeneous. The resulting

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solution can be passed through sodiated 4A molecular sieves. The solution can be returned to a double planetary mixer equipped with the propeller mixer and about 5 grams of polyethylene oxide (number average molecular weight about 600,000 available as Polyox WSR-205 from Union Carbide Chemicals and Plastics, Danbury, CT) can be added to the solution vortex by a mini-sieve such as a 25 mesh mini-sieve commercially available as Order No. 57333-965 from VWR Scientific, San Francisco, CA.

The solution can be heated while stirring until the temperature of the solution reaches 65°C. At this point, stirring can be continued until the solution is completely clear. The propeller blade can be removed and poly(N-methylpyrrole) can be added. The resulting mixture can be mixed at a rate of 7.5 cycles per second for 30 minutes in the double planetary mixer. During this mixing the temperature can slowly increase to a maximum of 73°C. At this point, the mixing can be reduced to 1 cycle per second and the mixture can be slowly cooled to a temperature of from 40°C to 48°C, e.g., about 45°C. The resulting cathode paste can be maintained at this temperature until just prior to application onto the current collector.

The resulting cathode paste can have the following approximate weight percent of components:

V ₂ O ₅	45 weight
percent	
Poly(N-methylpyrrole)	10 weight
percent	
4:1 propylene carbonate/tri-glyme	34 weight
percent	
polyethylene oxide	1 weight
percent	
polyethylene glycol diacrylate	8.5 weight
percent	
ethoxylated trimethylol-	

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propane triacrylate
percent

1.5 weight

5 In an alternative embodiment, the requisite amounts of all of the solid components can be added directly to the combined liquid components. In this regard, mixing speeds can be adjusted to account for the amount of the material mixed and size of vessel used to prepare the cathode paste. Such adjustments are well known to the skilled artisan.

10 The cathode paste noted above can be placed onto the adhesion layer of the current collector described above by extrusion at a temperature of from about 45° to about 48°C. A Mylar cover sheet can be placed over the paste and the paste can be spread to a thickness of
15 about 90 microns (μm) with a conventional plate and roller system and can be cured by continuously passing the sheet through an electron beam apparatus (Electrocurtain, Energy Science Inc., Woburn, MA) at a voltage of about 175 kV and a current of about 1.0 mA and at a
20 rate of about 1 cm/sec. After curing, the Mylar sheet can be removed to provide for a solid cathode laminated to the aluminum current collector described above.

C. Electrolyte

25 56 grams of propylene carbonate, 14 grams of triglyme, and 17 grams of urethane acrylate (Photomer 6140, available from Harckos, Manchester, U.K.) can be combined at room temperature until homogeneous. The resulting solution can be passed through a column of 4A
30 sodiated molecular sieves to remove water and then can be mixed at room temperature until homogeneous.

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At this point, 3 grams of polyethylene oxide having a number average molecular weight of about 600,000 available as Polyox WSR-205 from Union Carbide Chemicals and Plastics, Danbury, CT, can be added to the solution and then dispersed while stirring with a magnetic stirrer over a period of about 120 minutes. After dispersion, the solution can be heated to between 60°C and 65°C with stirring until the viscosifying agent dissolves. The solution can be cooled to a temperature of between 45° and 48°C, a thermocouple can be placed at the edge of the vortex created by the magnetic stirrer to monitor solution temperature, and then 10 grams of LiPF_6 can be added to the solution over a 120 minute period while thoroughly mixing to ensure a substantially uniform temperature profile throughout the solution. Cooling can be applied as necessary to maintain the temperature of the solution between 45° and 48°C.

In one embodiment, the polyethylene oxide can be added to the solution via a mini-sieve such as a 25 mesh mini-sieve commercially available as Order No. 57333-965 from VWR Scientific, San Francisco, CA.

The resulting solution should contain the following:

25	<u>Component</u>	<u>Amount</u>	<u>Weight Percent</u>
	Propylene Carbonate	56 g	56
	Triglyme	14 g	14
	Urethane Acrylate	17 g	17
	LiPF_6	10 g	10
30	PEO	3 g	3
	Total	100 g	100

= weight percent based on the total weight of the electrolyte solution (100 g)

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5 Optionally, solutions which can be produced as above and which contain the prepolymer, the polyethylene oxide viscosifier, the electrolyte solvent and the LiPF_6 salt can be filtered to remove any solid particles or gels remaining in the solution. One suitable filter device is a sintered stainless steel screen having a pore size between 1 and 50 μm at 100% efficiency.

10 Alternatively, the electrolyte solution can be prepared in the following manner. Specifically, in this example, the mixing procedure can be conducted using the following weight percent of components:

15	Propylene Carbonate	52 weight percent
	Triglyme	13 weight percent
	Urethane Acrylate ^b	20 weight percent
	LiPF_6	10 weight percent
	PEO ^c	5 weight percent

^b (Photomer 6140, available from Harckos, Manchester, U.K.)

20 ^c polyethylene oxide having a number average molecular weight of about 600,000 (available as Polyox WSR-205 from Union Carbide Chemicals and Plastics, Danbury, CT.)

The mixing procedure employs the following steps:

- 25 1. Check the moisture level of the urethane acrylate. If the moisture level is less than 100 ppm water, proceed to step 2. If not, then first dissolve the urethane acrylate at room temperature, $<30^\circ\text{C}$, in the propylene carbonate and triglyme and dry the
- 30 solution over sodiated 4A molecular sieves (Grade 514, 8-12 Mesh from Schoofs Inc., Moraga, CA) and then proceed to step 4.

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2. Dry the propylene carbonate and triglyme over sodiated 4Å molecular sieves (Grade 514, 8-12 Mesh from Schoofs Inc., Moraga, CA).

5 3. At room temperature, <30°C, add the urethane acrylate to the solvent prepared in step 2. Stir at 300 rpm until the resin is completely dissolved. The solution should be clear and colorless.

10 4. Dry and then sift the polyethylene oxide through a 25 mesh mini-sieve commercially available as Order No. 57333-965 from VWR Scientific, San Francisco, CA. While stirring at 300 rpm, add the dried and pre-sifted polyethylene oxide slowing to the solution. The polyethylene oxide should be sifted into the center of the vortex formed by the stirring means over a 30
15 minute period. Addition of the polyethylene oxide should be dispersive and, during addition, the temperature should be maintained at room temperature (<30°C).

20 5. After final addition of the polyethylene oxide, stir an additional 30 minutes to ensure that the viscosifier is substantially dispersed.

25 6. Heat the mixture to 68°C to 75°C and stir until the viscosifier has melted and the solution has become transparent to light yellow in color. Optionally, in this step, the mixture is heated to 65°C to 68°C.

30 7. Cool the solution produced in step 6 and when the temperature of the solution reaches 40°C, add the LiPF₆ salt very slowly making sure that the maximum temperature does not exceed 55°C.

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8. After the final addition of the LiPF_6 salt, stir for an additional 30 minutes, degas, and let sit overnight and cool.

5 9. Filter the solution through a sintered stainless steel screen having a pore size between 1 and 50 μm at 100% efficiency.

At all times, the temperature of the solution should be monitored with a thermocouple which should be placed in the vortex formed by the mixer.

10 Afterwards, the electrolyte mixture is then coated by a conventional knife blade to a thickness of about 50 μm onto the surface of the cathode sheet prepared as above (on the side opposite that of the current collector) but without the Mylar covering. The
15 electrolyte should be cured by continuously passing the sheet through an electron beam apparatus (Electrocurtain, Energy Science Inc., Woburn, MA) at a voltage of about 175 kV and a current of about 1.0 mA and at a conveyor speed setting of 50 which provides
20 for a conveyor speed of about 1 cm/sec. After curing, a composite can be recovered which contains a solid electrolyte laminated to a solid cathode.

D. Anode

25 The anode can comprise a sheet of lithium foil (about 51-76 μm thick) which is commercially available from FMC Corporation Lithium Division, Bessemer City, North Carolina

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E. The Solid Electrolytic Cell

A sheet comprising a solid battery can be prepared by laminating the lithium foil anode to the surface of the electrolyte in the sheet produced in step C above.

5 Lamination can be accomplished by minimal pressure.

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WHAT IS CLAIMED IS:

1. A cathode for an electrolytic cell which comprises:

a solid matrix forming monomer;

a cathodic material;

an electroconductive material consisting of a conducting polymer;

a solvent; and

a viscosifier.

2. The cathode of Claim 1, wherein the conducting polymer is polypyrrole, polyacetylene, polyazine, polyaniline, polyparaphenylene or polythiophene.

3. The cathode of Claim 1, having from about 10 to about 50 weight percent solvent, based on the total weight of the cathode composition.

4. The cathode of Claim 1, having from about 5 to about 30 weight percent solid matrix forming monomer, based on the total weight of the cathode composition.

5. The cathode of Claim 1, having from about 1 to about 20 weight percent viscosifier, based on the total weight of the cathode composition.

6. The cathode of Claim 1, having from about 1 to about 20 weight percent electroconductive material consisting of a conducting polymer, based on the total weight of the cathode composition.

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7. The cathode of Claim 1, having from about 35 to about 65 weight percent cathodic material, based on the total weight of the cathode composition.

5 8. A solid cathode which is a cured reaction product of the cathode composition of Claim 1.

9. The solid cathode of Claim 8, wherein the cured cathode has a thickness of from about 20 to about 120 microns.

10 10. An electrolytic cell which comprises:
an anode containing a compatible anodic material;
a cathode which comprises a solid polymeric
matrix,
a cathodic material, an electroconductive material
consisting of a conducting polymer, a solvent and a
15 viscosifier; and
interposed therebetween a solid, solvent-
containing electrolyte.

20 11. The electrolytic cell of Claim 11, wherein the conducting polymer is polypyrrole, polyacetylene, polyazine, polyaniline, polyparaphenylene or polythiophene.

12. A process for preparing a solid cathode for an electrolytic cell which comprises:

- 25 (a) providing a substrate;
(b) coating said substrate with a cathodic composition comprising: a solid matrix forming monomer, a cathodic material, an electroconductive material consisting of a conducting polymer, a solvent and a viscosifier; and
30 (c) curing said cathodic composition to provide a solid cathode.

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13. The process of Claim 12, wherein the conducting polymer is polypyrrole, polyacetylene, polyazine, polyaniline, polyparaphenylene or polythiophene.

5 14. A process for preparing an electrolytic cell which comprises:

(a) providing an anode containing a compatible anodic material;

10 (b) providing a cathode comprising a solid polymeric matrix, a cathodic material, an electroconductive material consisting of a conducting polymer, a solvent and a viscosifier;

(c) interposing between surfaces of the cathode and the anode an electrolyte composition; and

15 (d) curing said electrolyte composition so as to provide a solid electrolyte bonded to the surfaces of both the anode and cathode.

20 15. The process of Claim 14, wherein the conducting polymer is polypyrrole, polyacetylene, polyazine, polyaniline, polyparaphenylene or polythiophene.

INTERNATIONAL SEARCH REPORT

international application No.
PCT/US94/13734

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) :H01M 4/02, 4/04, 6/18

US CL : 429/215; 29/623.5; 429/192

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 429/192, 215, 217; 29/623.5

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X, P	US, A, 5,340,368 (KOKSBANG ET AL) 23 August 1994, see the Abstract, column 6, lines 43-68, column 11, line 14-column 13, line 66.	1-15
A, P	US, A, 5,330,856 (GONZALEZ) 19 July 1994	



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"E" earlier document published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"&" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

06 APRIL 1995

Date of mailing of the international search report

17 APR 1995

Name and mailing address of the ISA/US
Commissioner of Patents and Trademarks
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Form PCT/ISA/210 (second sheet)(July 1992)*

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US94/13734

Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This international report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☐ Claims Nos.:
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
3. ☐ Claims Nos.:
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

- I. Claims 1-9, 12 and 13, drawn to a cathode/method of making a cathode.
 - II. Claims 10-11, 14-15, drawn to an electrolytic cell/method of making a cell.
- The above inventions lack unity under PCT Rule 13 in that they lack a common special technical feature. For example, the Group II claims comprise materially different steps such as providing an anode layer and an electrolyte layer and forming a cell provided with these layers whereas the Group I claims are directed solely to a cathode of a different material.

1. ☒ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest.
- ☒ No protest accompanied the payment of additional search fees.

Form PCT/ISA/210 (continuation of first sheet(1))(July 1992)*

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